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A MULTIPLE Space and Time scale Approach for the quaNTification of deep saline formations for CO₂ storaGe

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TITLE: Modeling of pressure buildup and estimation of maximum injection rate for geological CO₂ storage at the South Scania site, Sweden

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1 **Modeling of pressure buildup and estimation of maximum injection**
2 **rate for geological CO₂ storage at the South Scania site, Sweden**

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1 Abstract. Carbon dioxide (CO₂) injection in deep saline formations causes pressure
2 increase which may be detrimental to the mechanical integrity of the storage reservoir.
3 Injection induced pressure buildup is a limiting factor for CO₂ injection rates and storage
4 capacity. In this study, we extend a semi-analytical solution (based on one-dimensional,
5 two-phase, two-component radial flow) for application to estimate pressure buildup and
6 maximum injection rate of CO₂ at a field site (South Scania, Sweden) using the method
7 of superposition of image well solutions to account for the straight-line boundaries
8 imposed by three fault zones. The semi-analytical approach for estimating pressure
9 buildup is validated by comparison to numerical simulations based on TOUGH2-ECO2N.
10 We analyze injection pressure sensitivity due to uncertainty in reservoir parameters as
11 well as boundary conditions. Maximum injection rates and pressure limited capacity
12 estimates are presented. This work demonstrates the use of semi-analytical solutions to
13 analyze pressure limitation on storage capacity for realistic reservoirs with irregular (non-
14 circular) boundaries. It is also shown that the semi-analytical approach can also be used
15 to evaluate the benefit of having multiple injection wells in terms of increasing the
16 injection-pressure-limited storage capacity. The methodology presented in this study is
17 useful for screening analysis of storage sites as well as for operation design and
18 optimization where pressure buildup as a limiting factor influences the objective function.
19 **Keywords:** Geological storage; Pressure-limited capacity; Numerical modeling;
20 Analytical solution; Mechanical failure.

1 **1. Introduction**

2 Reduction of atmospheric greenhouse gas concentrations can be achieved by carbon
3 capture and storage (CCS). Implementation of CCS requires sequestering a large amount
4 of carbon dioxide (CO₂) preferably in the deep saline formations. For closed formations,
5 the pore space needed for storing CO₂ is accommodated by enlargement of the rock pore
6 space and at the same time reduction in the volume of the formation fluid, through
7 compression of the rock material and the formation fluid, respectively. ¹ For semi-closed
8 or open formations, pore space accommodation of the injected CO₂ can be further
9 facilitated by the displacement of the native fluid from the storage formation into
10 overlying and underlying layers through brine leakage or into regions far away from the
11 injection zone. Pore space for storing CO₂ can be even created by production of the
12 native fluid. In any case, pressure perturbation in the host formation will be induced by
13 commercial scale geological storage of CO₂. This can result in direct adverse impact on
14 the mechanical integrity of the storage formation or may even have major secondary
15 effects of concern on the near-surface (fresh water) aquifers. Specifically, injecting a
16 large volume of CO₂ induces large scale pore pressure buildup and associated change in
17 the stress status, which may become a limiting factor for the CO₂ storage capacity
18 because (i) tensile or shear failure of the caprock may take place, (ii) existing fractures
19 and faults may be reactivated, and (iii) large-scale brine displacement into fresh-water
20 aquifers or brine leakage through abandoned well or fault zones may be induced, even if
21 the injected CO₂ is safely trapped. Birkholzer and Zhou ² argued that the basin-scale
22 hydrogeological impacts (i.e., due to pressure buildup and brine displacement, and
23 associated impacts on the environment) should be taken into account for the regional and

1 global capacity estimation, which typically has been based on simple calculation of the
2 fraction of the total reservoir pore space.³ In this study, we focus on modeling and
3 analyzing the pressure buildup that imposes restrictions of the injection rate due to
4 potential mechanical failure and the implication for capacity estimates.

5 Together with CO₂ injection and plume migration, pressure buildup in a storage
6 formation due to injection can be analyzed through numerical modeling using general
7 three-dimensional multiphase flow simulators such as TOUGH2-ECO2N⁴⁻⁶ and
8 PFLOTRAN.⁷ For example, Zhou et al.⁸ performed numerical modelling for CO₂
9 injection in the Mount Simon aquifer in the Illinois Basin using the parallel version of the
10 TOUGH2 simulator. They simulated CO₂ injection at a rate of 5Mt/year/well with a total
11 number of 20 wells, and found that the simulated pressure buildup in the core injection
12 area is about 35 bars which is not expected to affect the caprock geomechanical integrity.
13 Yamamoto et al.⁹ conducted high resolution numerical simulations for CO₂ storage in
14 the Tokyo Bay with a special focus on the large-scale pressure perturbation and the
15 associated shallow subsurface groundwater migration. Their results suggest that
16 groundwater pressure in the shallow confined aquifers can increase a few bars over
17 extensive regions. Birkholzer et al.¹⁰ numerically investigated the fluid pressure response
18 to CO₂ injection in a generic stratified system and concluded that large-scale pressure
19 change has more impact on groundwater resources than changes in water quality caused
20 by the migration of displaced brine. The above studies have employed full hydrodynamic
21 modelling and taken into account both the plume- and basin-scale processes related to
22 CO₂ injection, which requires a significant amount of computational resources. For
23 evaluation of large-scale impact of pressure perturbation, simpler and computationally

1 less expensive numerical models can also be used. These models include vertically
2 integrated two-phase flow numerical models^{11,12} and single-phase numerical models.¹³⁻¹⁵
3 Recent studies have also compared the performance of the numerical models of varying
4 levels of complexity.^{14,16,17} It has been shown in these studies that single-phase
5 numerical models may be adequate for prediction of large-scale pressure perturbation and
6 assessment of the area of review. However, when the possible mechanical failure is of
7 concern, single-phase models will lead to considerable inaccuracy in the estimation of
8 pressure change near the injection well due to the significant viscosity ratio between
9 supercritical CO₂ and brine and the evolution of dry-out zone and two-phase flow zone.

10 In contrast to numerical models, analytical methods allow for rapid evaluation and can
11 be employed to study parameter sensitivity for quick site screening and characterization.
12 Semi-analytical solutions^{1,18-22} have been developed to solve the radially symmetric two-
13 phase flow equations for CO₂ saturation and pressure distribution. Each of the analytical
14 methods involves a different set of simplifying assumptions. Some of the usual
15 assumptions include radially symmetrical domain, no-flow top and bottom boundary,
16 negligible capillary pressure, incompressible and immiscible flow, constant fluid and
17 rock properties, linear relative permeability functions etc. Since the compressibility of
18 CO₂ can be one or two orders of magnitude larger than that of brine for typical injection
19 depth, the assumption of constant CO₂ density may lead to notable errors in the
20 calculation of pressure evolution and CO₂ plume shape. In the models of Vilarrasa et
21 al.,^{21,22} CO₂ compressibility was explicitly accounted for, which is advantageous. The
22 considerable variation of CO₂ properties (i.e., density, viscosity etc.) due to fluid pressure
23 evolution may alternatively be remedied by calculating the fluid properties based on the

1 equations of state using the final pressure. This can be done by a simple iterative
2 procedure. Mathias et al.¹⁹ presented an analytical solution of pressure buildup taking
3 into account the effect of closed lateral boundary and partial miscibility between CO₂ and
4 brine, ignoring vertical flow of CO₂. It was found that the effect of brine evaporation can
5 be considerable while the effect of CO₂ dissolution is small. Mathias et al.²³ investigated
6 the sensitivity of estimating maximum sustainable injection rate to uncertain non-linear
7 relative permeability parameters.

8 The CO₂ injection is restricted by the maximum allowable pressure buildup (i.e., the
9 critical pressure buildup to induce tensile failure or fault reactivation), accurate
10 determination of which requires large-scale numerical modeling of the coupled
11 hydromechanical (HM) behaviour.²⁴⁻²⁸ Coupled HM modeling also needs detailed data
12 on mechanical properties of rock units. In many cases of site screening and
13 characterization, however, this detailed information may not be available and simplified
14 analysis for the maximum sustainable injection pressure can be performed.²⁹

15 In this paper, we will use both numerical modeling (based on TOUGH2-ECO2N) and
16 a semi-analytical solution (extended from Mathias et al.)^{19,23} to investigate the near-well
17 pressure buildup and thus the maximum allowable injection rate under different injection
18 scenarios for the South Scania site, south Sweden. We will also test injection pressure
19 sensitivity due to uncertainty in fluid and rock parameters as well as boundary conditions.
20 Maximum injection rates and pressure limited capacity estimates based on the modeling
21 results will be presented.

1 **2. Methods**

2 In this section, we describe two hydrodynamic modeling methods for pressure buildup,
3 one based on numerical modeling and the other based on a semi-analytical solution. We
4 also provide descriptions on how we estimate the maximum sustainable injection
5 pressure and the maximum injection rate.

6 **2.1. Numerical modeling**

7 Injection and migration of CO₂ into brine formations present a two-phase flow
8 problem. In this study, numerical simulations are conducted using the multiphase flow
9 simulator TOUGH2⁴ with the equation-of-state module ECO2N.⁵ ECO2N is a fluid
10 property module designed for applications to geologic sequestration of CO₂ in saline
11 aquifers. It describes the thermodynamics and thermophysical properties of H₂O - NaCl -
12 CO₂ mixtures, and accurately reproduces fluid properties for the temperature, pressure
13 and salinity conditions of interest for geological sequestration. Local equilibrium
14 solubility is applied to treat phase partitioning between the aqueous and the CO₂-rich
15 phase as well as to handle dissolution or precipitation of salt. For details of the numerical
16 model, refer to the manuals.^{4,5}

17 **2.2. Analytical methods for pressure buildup**

18 The analytical modeling approach for pressure buildup in this study is based on the
19 semi-analytical solution developed by Mathias et al.^{19,23} Here, we extend the solution by
20 including superposition of pressure response from imaginary image wells to take into
21 account the effect of the fault boundaries. Strictly speaking, the approach of superposition
22 is limited to linear systems. This requirement is not satisfied in the two-phase region

1 where CO₂ and brine coexist. However, as will be shown later, the two-phase region is
 2 small compared to the extent of the pressure response, which justifies the use of the
 3 superposition approach.

4 Under reservoir conditions, supercritical CO₂ can partially dissolve into brine and at
 5 the same time water can partially vaporize in the presence of CO₂. This partial miscibility
 6 gives rise to complex flow regimes and dynamics for the evaluation of pressure response.
 7 Assuming vertical pressure equilibrium, constant fluid properties, negligible capillary
 8 pressure and equilibrium dissolution between CO₂ and water, Mathias et al.¹⁹ solved the
 9 relevant (radially symmetric) governing equations describing the above flow
 10 characteristics. It is possible to obtain closed-form solutions for the gas saturation and
 11 pressure for the case with linear relative permeability functions. For nonlinear relative
 12 permeability functions, numerical evaluation of the gas saturation at the leading shock
 13 front needs to be used, and the solution becomes semi-analytical. Note that wellbore skin
 14 effect is not considered.

15 The analytical model¹⁹ can be applied to both laterally open and closed aquifers. It can
 16 be summarized as:

$$\begin{aligned}
 \Delta P = P - P_{ini} = & \\
 \frac{M_0}{4\pi\rho_g Hk} & \begin{cases} \mu_g q_{D1} \ln(z_T/z)/k_{rs} + \mu_g q_{D2} F_2(z_T) + \mu_b q_{D3} F_1(z_L), & 0 \leq z < z_T \\ \mu_g q_{D2} F_2(z) + \mu_b q_{D3} F_1(z_L), & z_T \leq z < z_L \\ \mu_b q_{D3} F_1(z), & z \geq z_L \end{cases} \quad (1)
 \end{aligned}$$

17 where ΔP is the pressure buildup,
 18 P is the vertically averaged pressure,
 19 P_{ini} is the initial pressure (vertically averaged),
 20 M_0 is the mass injection rate of CO₂,

1 ρ_g is the density of CO₂,
 2 μ_g is the viscosity of CO₂,
 3 k is the permeability of the formation,
 4 H is the thickness of the formation,
 5 k_{rs} is the permeability reduction factor due to salt precipitation,
 6 μ_b is the viscosity of the brine,
 7 q_{D1} , q_{D2} , and q_{D3} are the dimensionless, piecewise total fluxes, which can be obtained
 8 from Equations (27) and (28) in Mathias et al.¹⁹
 9 z is the similarity transform variable for time t and radial distance r

$$z = \frac{\pi\phi\rho_g Hr^2}{M_0 t},$$

11 and z_T and z_L are locations of the trailing and leading shocks in similarity space, which
 12 can be evaluated from Equations (30-35 and 53) in Mathias et al.¹⁹. In Equation (1), $0 \leq z$
 13 $< z_T$ corresponds to the dry-out zone in physical space; $z_T \leq z < z_L$ corresponds to the two-
 14 phase region where CO₂ and brine coexist; and $z > z_L$ corresponds to the single-phase
 15 region occupied by the native brine. The solution for pressure response reduces to one
 16 that is based on single-phase flow when the radial distance r is larger than the extent of
 17 CO₂ plume (i.e., $z > z_L$).

18 In Equation (1),

$$F_1(z) = \begin{cases} (\alpha z_E)^{-1} - \frac{3}{2} + \ln\left(\frac{z_E}{z}\right) + \frac{z - z_L}{z_E}, & z_E < \frac{0.5615}{\alpha} \\ E_1(\alpha z), & z_E > 0.5615/\alpha \end{cases} \quad (2)$$

20 with

$$1 \quad \alpha = \frac{M_0 \mu_b (c_r + c_b)}{4\pi \rho_g H k}, \quad (3)$$

$$2 \quad F_2(z) = -\frac{1}{\mu_g} \int_z^{z_L} \left(\frac{k_{ra}}{\mu_b} + \frac{k_{rg}}{\mu_g} \right)^{-1} \frac{1}{z} dz \quad (4)$$

3 where ρ_b is the density of the native brine,

4 z_E is similarity transform for the radial extent of the formation r_E ,

5 k_{ra} and k_{rg} are the relative permeabilities of the aqueous phase and gas phase,

6 respectively,

7 and c_r and c_b are the compressibilities of rock pores and brine, respectively.

8 Note that the fluid densities, viscosities and mass fractions in each phase are all
 9 functions of pressure and thus vary as pressure builds up in the formation. For estimating
 10 pressure buildup, these parameters need to be iteratively determined. In this study, we
 11 iteratively solve for pressure buildup by using Equation (1) and updating the parameters
 12 based on the equations of state for CO₂ and brine offered in ECO2N which uses the
 13 Altunin³⁰ correlation implemented as a look-up table.

14 To account for the effect of closed formation boundaries, we calculate the additional
 15 pressure increase due to the no-flow boundaries by introducing image wells. The image
 16 wells (fictitious injection wells), having the same injection rate M_0 as the real injection
 17 well, are placed at locations to create symmetry along no-flow boundaries in the flow
 18 field of fictitious unbounded reservoir. The additional pressure increase (ΔP_f) is
 19 calculated as:

$$20 \quad \Delta P_f = \sum_{i=1}^{n_{im}} \Delta P_i(r_i, t) \quad (5)$$

1 where n_{im} is the number of image wells, and $\Delta P_f(r_i, t)$ is the pressure buildup contribution
2 (calculated by Equation 1) from the i th image well with a distance r_i from the actual
3 injection well.

4 If we consider multiple real injection wells distributed over a modeling domain, the
5 pressure perturbation from each well will interfere with that from the surrounding wells.
6 As a result, the wells that are not close to the open domain boundaries will effectively
7 behave as if they were surrounded by a no-flow boundary. Therefore, in the modeling of
8 pressure buildup in the vicinity of the injection wells, we consider a closed domain for
9 each individual injector with an equivalent domain radial extent r_E determined by the
10 total domain area A and the number of injection wells n_w , that is, $r_E = (A/\pi n_w)^{0.5}$.

11 **2.3. Maximum sustainable injection pressure**

12 Accurate estimation of the maximum sustainable injection pressure (or the injection
13 pressure threshold, P_{th}) would require detailed knowledge of *in situ* stresses and couple
14 flow/mechanical numerical modeling. Due to the lack of information of the stress status
15 for the study site, we resort to simplified analysis to obtain the maximum sustainable
16 injection pressure P_{th} , similar to Rutqvist et al.²⁶ and Mathias et al.²⁹ We estimate the
17 initial vertical stress from the weight of the overburden rock, assuming an average
18 saturated rock density of 2260 kg/m^3 . This gives an initial vertical stress $\sigma_z = 3.77 \times 10^7 \text{ Pa}$
19 at a depth of 1700 m. We consider two initial stress regimes: an extensional stress regime
20 with stress ratio between the minimum horizontal stress and the vertical stress $\sigma_h / \sigma_z =$
21 0.7 and a compressional stress regime with $\sigma_h / \sigma_z = 1.5$. For the case of $\sigma_h / \sigma_z = 0.7$,
22 according to Mathias et al.,²⁹ the threshold pressure is constrained by the fracturing
23 pressure, which can be conservatively estimated as the minimum principle stress (i.e., P_{th}

1 = $0.7\sigma_z$). For the case of $\sigma_h / \sigma_z = 1.5$, the fracturing pressure can be estimated to be equal
2 to σ_z , while the critical pressure for slip (shear failure), P_s , assuming zero cohesion and a
3 friction angle of 30° , can be estimated from the Coulomb failure criterion as ²⁶

$$4 \quad P_s = \sigma_{m2} - 2|\tau_{m2}| \quad (6)$$

5 where σ_{m2} and τ_{m2} are the two-dimensional mean stress and maximum shear stress in the
6 (σ_h, σ_z) plane. This give a slip pressure $P_s = 0.75\sigma_z$, which is smaller than the fracturing
7 pressure and defines the pressure threshold P_{th} in this case. From the above analysis, we
8 can see that the pressure threshold may be determined by different failure modes under
9 different initial stress conditions. However, for the two cases of $\sigma_h / \sigma_z = 0.7$ and 1.5 , the
10 threshold pressure only differs to a small extent ($0.7\sigma_z$ and $0.75\sigma_z$). Thus, in this study,
11 we conservatively choose a threshold pressure value equal to $0.7\sigma_z$ which serves to
12 determine the maximum injection rate (M_{max}). This corresponds to a pressure of 2.64×10^7
13 Pa, or a 55% increase from the initial hydrostatic pressure 1.7×10^7 Pa.

14 **3. The South Scania site, Sweden**

15 We apply the modeling methods to the South Scania site, which is located in the
16 southwestern region of Sweden (see Fig. 1). A number of deep boreholes have been
17 drilled and several sandstone layers have been identified which constitute potential
18 candidates for geological storage of carbon dioxide. ³¹ These sandstone layers appear in
19 the Lower Cretaceous and Lower Jurassic sequences. In this study, we consider a storage
20 reservoir consisting of these layers (alternating sandstone and siltstone) within the depth
21 interval between 1650 m and 1725 m. The reservoir is bounded by three faults: the
22 Romeleåsen Fault Zone, the Svedala Fault and the Öresund Fault. These faults are
23 conceptualized into straight lines and shown in red in Fig. 1. The boundary conditions

1 associated with these faults are currently uncertain. However, available geological
2 information indicates that the Romeleåsen Fault is a regional complex system of reverse
3 faults limiting the sedimentary basin, i.e., the Danish Basin to the northeast. The fault
4 zone is, based on lithological and structural data, considered to provide a closed boundary
5 condition for the Lower Cretaceous and Lower Jurassic reservoirs. In this study, we will
6 examine the effect of boundary conditions on the pressure buildup. We assume a uniform
7 thickness for the reservoir and impermeable overlying and underlying formations. The
8 modeling is simplified to the case of a two-dimensional (vertically integrated) numerical
9 analysis. Based on the available site data, we assume a homogeneous permeability of
10 $1.0 \times 10^{-13} \text{ m}^2$ and a porosity of 0.15. The pore compressibility is taken as $4.5 \times 10^{-10} \text{ Pa}^{-1}$.
11 Since there is no site specific data on the capillary pressure and relative permeability
12 parameters, we choose the relevant parameters based on the Mt. Simon sandstones
13 measured by Krevor et al.³² We use the Brooks-Corey function³³ for capillary pressure
14 and the Brooks-Corey-Burdine function^{33,34} for relative permeability. Residual brine
15 saturation S_{wr} is taken as 0.22; residual gas saturation S_{gr} is 0.2; entry capillary pressure
16 is 4600 Pa; and the pore size distribution parameter is 0.55. A study on the effect of
17 heterogeneity on fluid migration and upscaling based on the South Scania site is
18 presented in Yang et al.³⁵ However, the effect of heterogeneity on pressure buildup will
19 not be discussed here. A more detailed description of the site can be found in Erlström et
20 al.³⁶

21 **4. Results**

22 In this section, we first show comparison between the pressure buildup prediction from
23 the TOUGH2-ECO2N simulations and from the semi-analytical solution. Then we

1 proceed to apply the semi-analytical solution to investigate the effect of operational
2 parameters (such as the number of injection wells) and boundary conditions, followed by
3 sensitivity of pressure prediction to intrinsic reservoir parameters (such as porosity,
4 permeability, rock compressibility, reservoir thickness, etc.). Note that the pressure
5 increase refers to the difference between injection pressure and initial hydrostatic
6 pressure at end of the injection period (50 years), unless otherwise stated.

7 **4.1. Comparison between numerical simulation and semi-analytical solution**

8 In order to validate the semi-analytical approach, we have numerically simulated
9 pressure response due to CO₂ injection in the formation for comparison. We assume
10 closed lateral boundaries imposed by the three fault zones. This boundary condition
11 corresponds to the case of highest possible pressure buildup in the formation because
12 there is no pressure dissipation induced by brine migration out the reservoir. Single well
13 injection at the location of FFC-1 has been modeled. Injection time is set as 50 years.
14 Injection rates ranging from 0.5 to 3.0 Mt/yr have been tested. The simulated CO₂ plume
15 for injection rate of 2.0 Mt/yr has a radius about 3 km, which is much smaller than the
16 flow domain with equivalent radius of 30 km. This also supports the use of the
17 superposition approach for pressure response. Since we focus on the pressure buildup
18 around the injection well, the CO₂ plume plots will not be shown and discussed. Fig. 2
19 shows the simulated pressure increase in the modeling domain for two injection rates.
20 When the injection rate is 1.0 Mt/yr, the pressure increase at the injection area is 63 bars;
21 when the injection rate is 2.0 Mt/yr, it grows to 120 bars. This almost linear behavior
22 suggests that the two-phase flow region (in between the dry-out zone and the single-
23 phase brine flow zone) does not impose significant non-linearity to the injection rate-

1 pressure response relationship, probably due to the fact that the two-phase region is much
2 smaller than the extent of the entire flow domain.

3 In this case of closed reservoir, we have two alternatives to apply the semi-analytical
4 solution. One is to conceptualize the reservoir into a disc shape with an equivalent radius
5 extent r_E for the reservoir based on the area. This yields an equivalent r_E of 30 km. The
6 other is to use superposition of image well solutions to represent the effect of closed
7 boundary conditions. The principle for placement of image wells is to create a fictitious
8 unbounded domain whose flow field has symmetry along the no-flow fault boundaries. It
9 should be noted that, for several linear faults intersected at arbitrary angles, finding the
10 appropriate number of locations of image wells can be a non-trivial task. Some examples
11 of how to consider image wells can be found in Ferris et al.³⁷ In this study, we consider
12 both primary and secondary image wells to take into account the effect of three fault
13 boundaries (Fig. 3a). Fig. 3b shows that the semi-analytical approach based on
14 superposition of image well solutions can reasonably well match the pressure prediction
15 based on numerical modeling. But there is appreciable differences between the semi-
16 analytical approach with area-equivalent reservoir radial extent and the numerical results;
17 when the injection rate is 1.5 Mt/yr, the pressure increase predicted by equivalent r_E
18 semi-analytical method shows a 14% deviation from the numerical counterpart. The
19 reason for this deviation is due to the fact that the actual distances from the injection well
20 to the boundaries are much smaller than the equivalent r_E of 30 km (the reservoir is
21 significantly non-circular shaped) so that a portion of the reservoir space is not
22 effectively used for pressure dissipation.

1 From this comparison analysis, it is evident that the semi-analytical method with
2 superposition of image well solutions can give adequate pressure prediction for a site
3 with linear fault boundaries. In the following, we will only use the analytical method for
4 modeling pressure buildup.

5 **4.2. Number of injection wells**

6 Number and locations of injection wells can be characterized as operational parameters
7 for deployment of large-scale CO₂ storage. They can have a significant impact on the
8 magnitude and spatial distribution of pressure buildup, because of which they should be
9 taken into account for optimal design of effective pressure management and thus storage
10 efficiency. In this section, we focus on the effect of number of injection wells on the
11 pressure buildup. To illustrate this, we assume closed boundaries for the three faults,
12 which corresponds to the boundary case of highest pressure buildup. We also assume that
13 wells are located in the center of each part of the divided reservoir domain. Each small
14 part is conceptualized to have an area-equivalent radial extent, $r_E = (A/\pi n_w)^{0.5}$, for
15 simplicity. Fig. 4 shows a schematic illustrating the scenario of multiple injection wells.

16 Pressure buildup for four different numbers of injection wells ($n_w = 1, 3, 5$ and 9) is
17 analyzed. Fig. 5 shows that the effect of the number of injectors on the well pressure
18 buildup is strongly dependent on the reservoir permeability. For low permeability ($k = 50$
19 mD), there is significant difference in well pressure between the single-well scenario and
20 nine-well scenario for the same total injection rate ($M_{tot} = M_o \times n_w$). The maximum
21 injection rate M_{max} for the single-well scenario is about 0.98 Mt/yr, whereas for the nine-
22 well scenario, M_{max} increases by a factor of more than 3 (3.2 Mt/yr). When the base-case
23 permeability ($k = 100$ mD) is considered, M_{max} increases by a factor of about 2.2 from the

1 case of $n_w = 1$ to the case of $n_w = 9$. When permeability is high ($k = 400$ mD), as shown
2 in Fig.5c, distributing the total injection rate to a larger number of injector does not seem
3 to decrease the well pressure buildup significantly. This is because the spatial distribution
4 of pressure buildup is more uniform (pressure perturbation travels farther, i.e., stronger
5 pressure interaction among different injection wells) when the permeability is higher.

6 From the above analysis, it can be seen that we can achieve a rate of at least 3 Mt/yr if
7 we have 9 wells, no matter the permeability is 50 or 400 mD. However, more injection
8 wells also require more operational cost for pipeline network, CO₂ transportation, drilling
9 cost, etc. Under the pressure-limited scenario, less injection wells are needed for a higher
10 reservoir permeability when the same amount of CO₂ is to be stored.

11 **4.3. Effect of boundary conditions**

12 The hydraulic properties and boundary conditions along the faults are not exactly known.
13 In order to assess the effect of boundary conditions on pressure buildup prediction, we
14 consider two extreme cases (one for all closed faults and the other for all open faults)
15 together with the case of only one closed fault (Romeleåsen). For the South Scania site,
16 by *open faults* it is meant that the formation continuity is not affected by the faults and
17 that the physical boundary for the reservoir would be at places where the formation
18 pinches out or outcrops. The two extreme cases provide a theoretical bound for pressure
19 buildup prediction for a given reservoir parameter set. We consider one injection well at
20 the location of FFC-1 and we use the semi-analytical method with superposition of image
21 well solutions to account for the effect of boundaries.

22 Fig. 5 shows that for the base case parameters listed in Sect. 3, the boundary conditions
23 can have a significant impact on the pressure buildup at the injection location. In terms of

1 the maximum allowed injection rate, the all-closed-faults case corresponds to a rate of 1.6
2 Mt/yr, while the number for the all-open-faults case is 2.7 Mt/yr. The case of all closed
3 faults decrease the injectivity by about 40% compared to the open boundary case. Fig.2
4 also shows that the pressure disturbance at the boundaries is significant at 50 years. In
5 fact, the time for the pressure disturbance to reach the boundary can be estimated by $t_{pb} =$
6 $L^2/4D_h$, where L is the distance from the injection well to boundary and D_h is the
7 hydraulic diffusivity, $D_h = k/\phi\mu_b(c_r + c_b)$. For the parameters given in Sect. 3 and a
8 distance of 25 km, t_{pb} is only about 4 years, much shorter than the injection period of 50
9 years. If the hydraulic diffusivity is smaller (e.g., by reducing permeability), the
10 boundaries would have less impact on the pressure buildup.

11 **4.4. Sensitivity to intrinsic reservoir parameters**

12 Even though rock properties (parameters) relevant to CO₂ injection and migration can
13 be estimated from field tests and laboratorial experiments on core samples, they can still
14 be considered to a large extent uncertain due to the typical existence of multi-scale
15 heterogeneity.^{38,39} The uncertainty of pressure buildup prediction due to relative
16 permeability parameters has been analyzed by Burton et al.⁴⁰ and Mathias et al.²³ In this
17 work, we perform sensitivity study of pressure buildup on parameters including
18 permeability, porosity, compressibility and reservoir thickness. We do this for two sets of
19 boundary conditions: the more probable case of only one impermeable fault (Romeleåsen)
20 according to available geological information and the unfavorable case of all closed
21 boundaries. One injection well at the FFC-1 location is considered. The method of
22 superposition of image well solutions is used. Note that when we vary a parameter we fix
23 all the other parameters to the base case values as specified in Sect. 3.

1 Formation permeability is the most sensitive parameter for pressure buildup for the
2 case of single injection well. Fig. 7 shows that the pressure increase exhibits a wide range
3 of values as permeability varies for both boundary scenarios. For example, in Fig. 7a, the
4 pressure increase changes from 25 to 253 bars as permeability decrease from 400 to 25
5 mD for an injection rate of 2 Mt/yr. In comparison to permeability, porosity is a much
6 less sensitive parameter for the pressure buildup. Additionally, the effect of porosity on
7 pressure is dependent on the boundary conditions, as shown in Fig. 8. In the boundary
8 scenario of only one impermeable fault (Fig. 8a), varying porosity leads to negligible
9 effect on pressure increase. This is partly due to the fact that realistic porosity variation is
10 typically small, within a factor of 2 or 3. The other part of the explanation can be argued
11 by the double roles of porosity on injection pressure buildup. For open reservoirs or
12 nearly open reservoirs (such as the one here with one impermeable fault), decreasing
13 porosity means less pore volume available for the compressibility (storativity) effect, but
14 at the same time it also increases hydraulic diffusivity and thus promotes outwards
15 migration of far-field brine. Fig. 8b shows that for the scenario of closed boundaries,
16 porosity can affect the pressure buildup. This is because the far-field migration of brine is
17 limited by the boundaries and the compressibility effect becomes visible. We expect the
18 effect of reservoir rock compressibility to play a similar role to that of porosity. However,
19 rock compressibility will typically have a larger variability than porosity. Fig. 9 presents
20 the effect of rock compressibility on the pressure increase with the compressibility varies
21 from $4.5 \times 10^{-9} \text{ Pa}^{-1}$ to $4.5 \times 10^{-11} \text{ Pa}^{-1}$. The effect of reservoir thickness on pressure buildup
22 is presented in Fig. 10. As expected from the semi-analytical solution, pressure increase
23 is inversely proportional to the reservoir thickness.

1 **4.5. Maximum injection rate and pressure limited capacity**

2 Based on the parametric sensitivity study, we determine maximum injection rates for
3 the different parameter sets by assigning a maximum allowable pressure increase of 94
4 bars (see Sect. 2.3) and looking up in the response of pressure increase to different
5 injection rates. Table 1 summarizes the results of maximum injection rates. In accordance
6 with the pressure buildup results, the maximum injection rate is most sensitive to
7 permeability variations and relatively insensitive to porosity variation. The pressure
8 limited capacity is then simply determined by multiplication of the maximum injection
9 rate and the injection duration (50 years). Given the base case parameters, pressure
10 buildup can limit the storage capacity to $2.4 \times 50 = 120$ Mt for the probable boundary
11 scenario of impermeable Romeleåsen fault zone. For the scenario of all faults
12 impermeable, the storage capacity becomes 80 Mt. If the formation permeability is 400
13 mD, the storage capacity for the scenario of impermeable Romeleåsen Fault Zone
14 increases considerably to 415 Mt.

15 **5. Discussion and concluding remarks**

16 In this study, we have extended a semi-analytical solution^{19,23} for application to
17 estimate pressure buildup and maximum injection rate of CO₂ at a field site (South
18 Scania, Sweden) using the method of superposition of image well solutions. The site is
19 characterized by three major faults formed into a triangular geometry. The semi-
20 analytical approach for estimating pressure buildup has been validated by comparison to
21 numerical simulations based on TOUGH2-ECO2N for the case of closed boundaries. We
22 have tested injection pressure sensitivity due to uncertainty in reservoir parameters as
23 well as boundary conditions. Maximum injection rates and pressure limited capacity

1 estimates based on the modeling results are presented. This work demonstrates the use of
2 semi-analytical solutions to analyze pressure limitation on storage capacity for realistic
3 reservoirs with irregular (non-circular) boundaries. The methodology is useful for
4 screening analysis of storage sites as well as for operation design and optimization where
5 pressure buildup as a limiting factor influences the objective function.

6 The semi-analytical solution is based on one-dimensional, two-phase, two-component
7 radial flow. It takes into account both the effect of mutual solubility between CO₂ and
8 brine and the effect of relative permeabilities. Since it is based on one-dimensional
9 equations, CO₂ migration due to buoyancy is ignored. For evenly distributed injection
10 rates along the formation thickness, buoyancy flow of CO₂ would cause the pressure
11 buildup to be higher at the top of the formation. However, this effect should be small
12 (maximum a few bars, given the thickness of the formation and the density difference
13 between CO₂ and brine) compared to the threshold pressure increase of $\sim 10^2$ bars.

14 Parametric sensitivity study using the semi-analytical model shows that the pressure
15 buildup for the case of single injection well is very sensitive to the formation
16 transmissivity (permeability and thickness) and boundary conditions. However, in many
17 field sites, permeability is largely uncertain due to heterogeneity and data scarcity. Also,
18 uncertainty can often exist in the boundaries conditions associated with the fault zones.
19 This means that appraisal of the practical storage capacity under the pressure constraint
20 should give uncertainty bounds, which can be obtained using the semi-analytical
21 approach.

22 For closed reservoirs, the semi-analytical approach can also be used to evaluate the
23 benefit of having more injection wells in terms of increasing the injection pressure

1 limited storage capacity. This is demonstrated for the South Scania site with the
2 impermeable faults scenario. Here, the reservoir domain is conceptualized as consisting
3 of individual parts with a closed circular boundary for each injection well. The
4 controlling factor for the effect of number of injection wells is the hydraulic diffusivity
5 D_h . If D_h is small (propagation distance of the pressure perturbation during the injection
6 period is small), increasing the number of injection wells leads to increased storage
7 capacity, although the additional operation cost needs also to be considered in the storage
8 project implementation.

9 It is worth noting that we have assumed impermeable sealing units for the storage
10 formation. In fact, the injection-induced pore pressure can be dissipated by brine storage in
11 and displacement through the caprock if the permeability of the caprock is not extremely
12 low and the compressibility of the caprock is large.¹⁴ Thus, accounting for the effect of
13 caprock and baserock could result in smaller pressure buildup and larger injection rates,
14 depending on the relevant parameters of the sealing units. In this regard, the pressure
15 limited capacity estimates for the South Scania site may be conservative. We are
16 currently working on extending the semi-analytical solution to account for the pressure
17 dissipation due to sealing rocks.

18 Storage capacity can be constrained both by pressure buildup and long term CO₂
19 plume migration to undesirable locations such as conducting faults and outcrop regions
20 (e.g., Szulczewski et al., 2014). We are carrying out dynamic modeling based on a more
21 detailed geological model to verify if the migration (space available for trapping)
22 constraint becomes for more dominant for a range of injection volumes.

23

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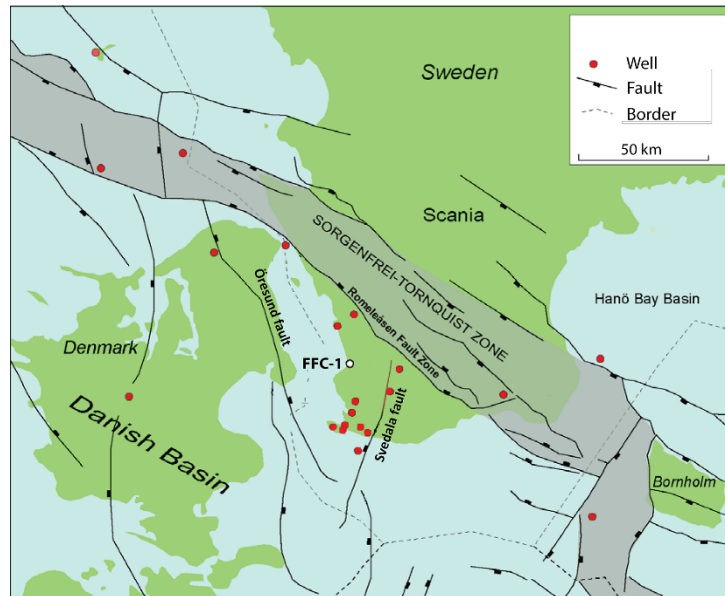
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1 **Table 1.** Sensitivity of maximum injection rate (Mt/yr) to parameters and boundary
 2 conditions.

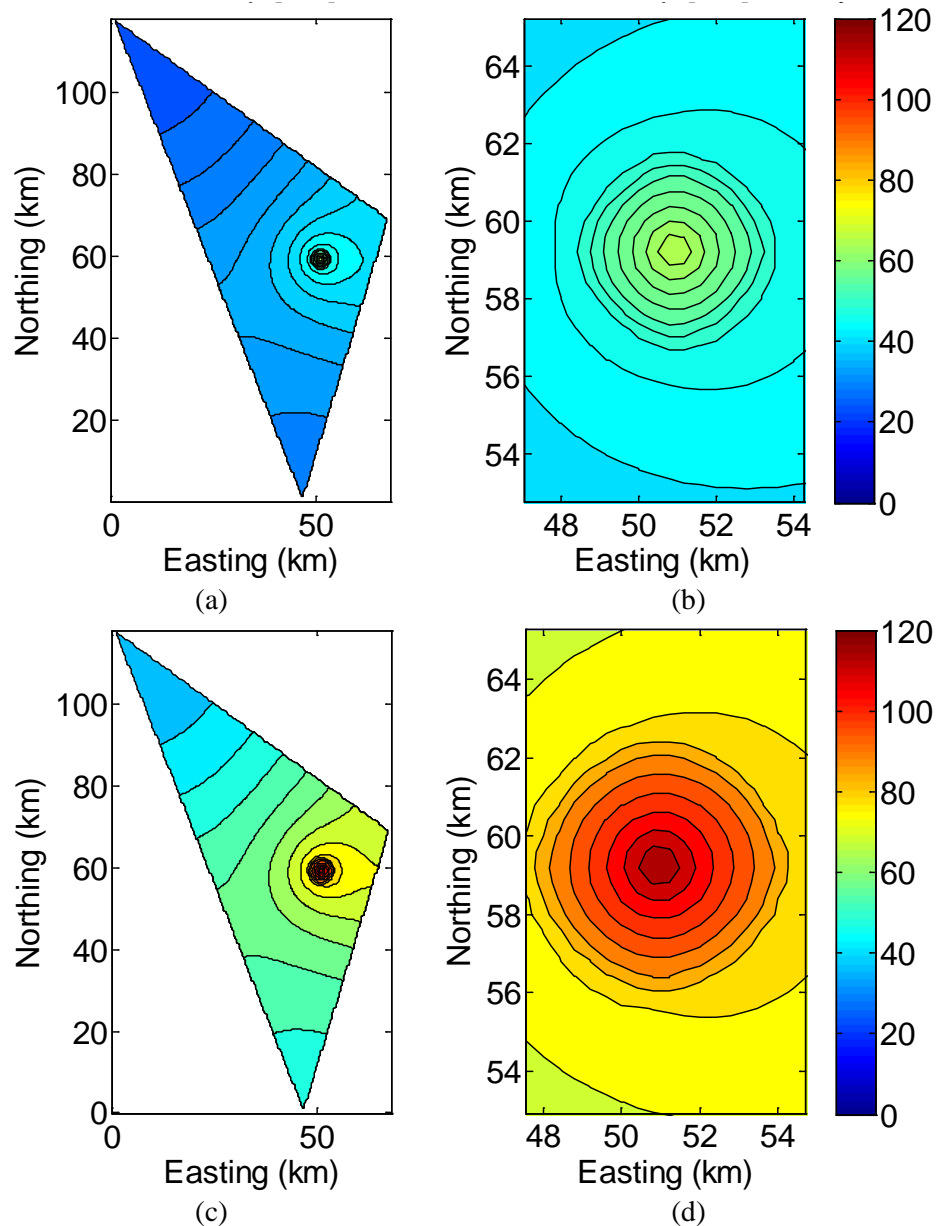
Parameter	Romeleåsen Fault impermeable	All faults impermeable
$k = 25$ mD	0.68	0.59
50 mD	1.3	0.98
100 mD *	2.4	1.6
400 mD	8.3	2.8
$\varphi = 0.1$	2.3	1.4
0.15 *	2.4	1.6
0.2	2.5	1.7
0.25	2.5	1.9
$c_r = 4.5 \times 10^{-9}$ Pa ⁻¹	2.2	1.3
4.5×10^{-10} Pa ⁻¹ *	2.4	1.6
4.5×10^{-11} Pa ⁻¹	3.1	2.8
$H = 50$ m	1.6	1.1
75 m *	2.4	1.6
100 m	3.2	2.2
150 m	4.8	3.2

3 * Base case parameters

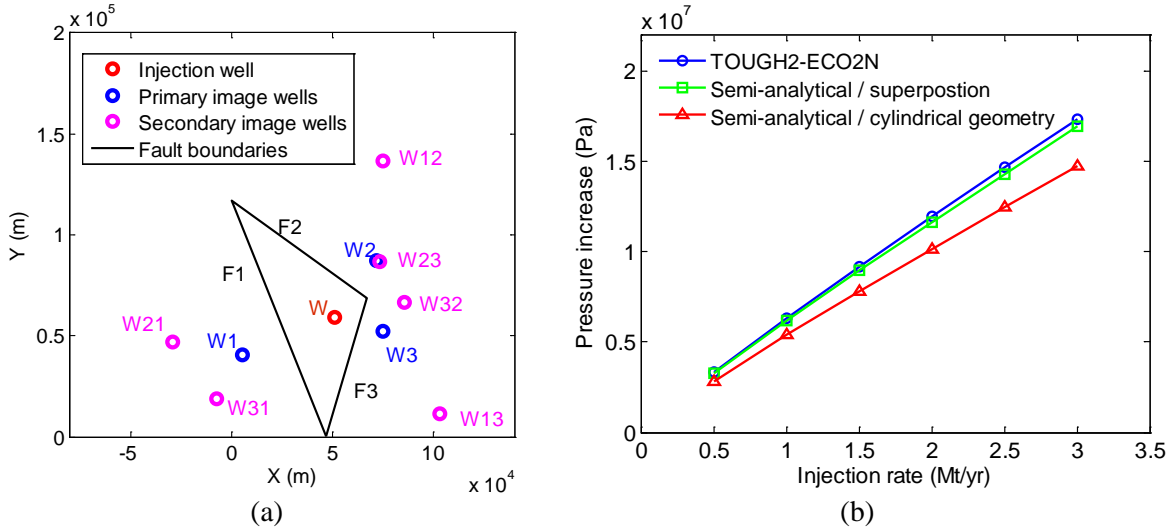


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 5 **Fig. 1.** Map of the South Scania site, Sweden.

6



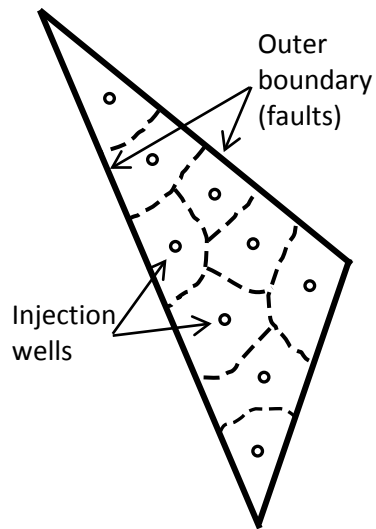
2 **Fig. 2.** (a) Numerically simulated pressure increase (bar) at 50 years with CO₂ injection
 3 rate 1 Mt/yr. (b) Zoom-in view (CO₂ injection rate 1 Mt/yr). (c) Numerically simulated
 4 pressure increase (bar) with CO₂ injection rate 2 Mt/yr. (b) Zoom-in view (CO₂ injection
 5 rate 2 Mt/yr).



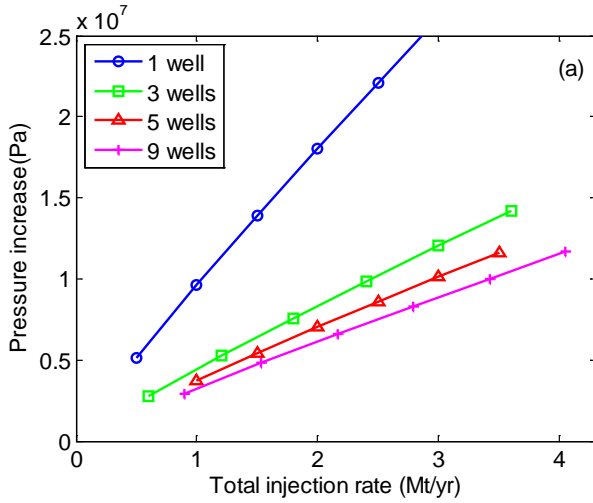
1 **Fig. 3.** (a) Reservoir modeling domain with fault boundaries and locations of the
 2 injection well and image wells. Primary image well W_i is the image of injection well with
 3 respect to fault F_i ; Secondary image well W_{ij} is the image of primary image well W_i with
 4 respect to fault F_j ; (b) Comparison of pressure prediction between numerical modeling
 5 and analytical solutions.

6

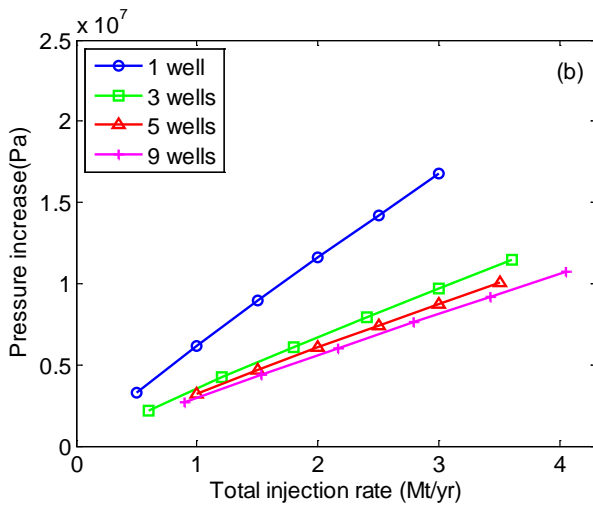
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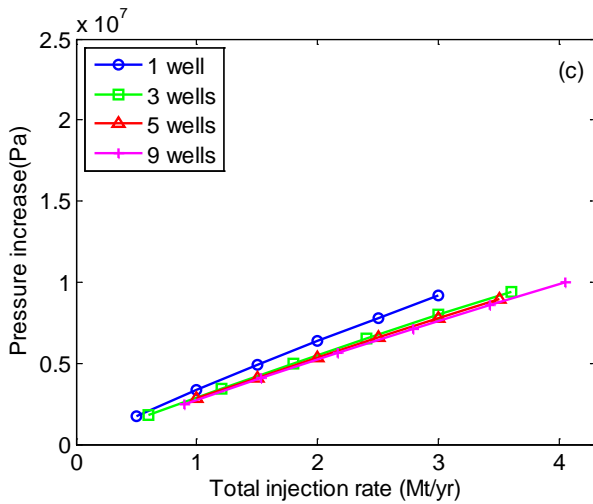
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2 **Fig. 4.** Schematic showing the divided reservoir domain with the scenario of multiple
3 injection wells.
4



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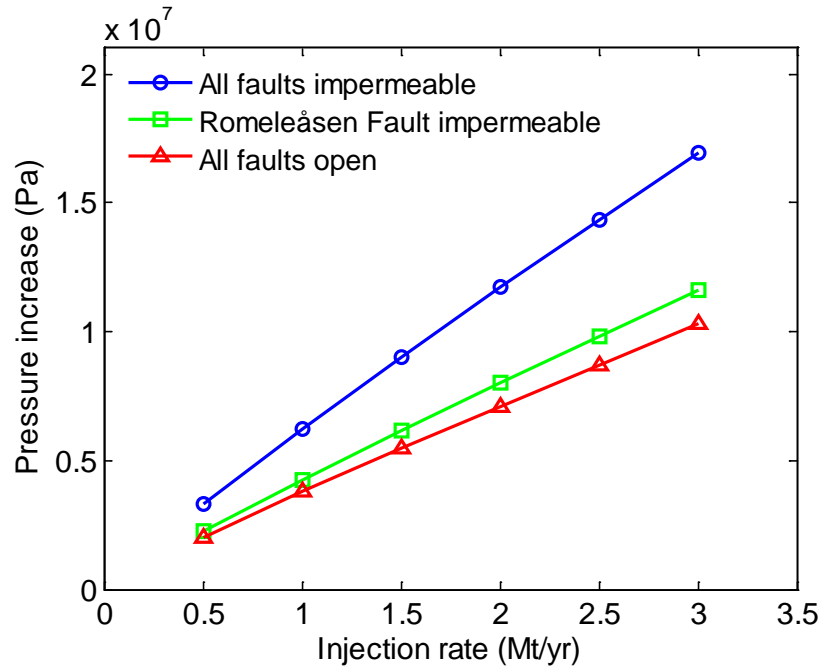


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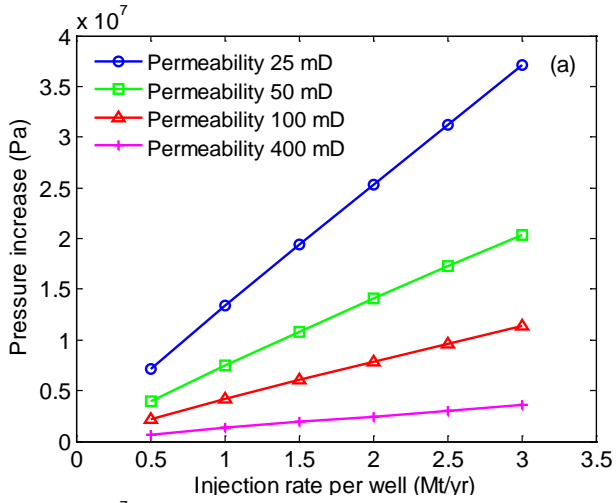
4 **Fig. 5.** Well pressure increase for different number of injection wells with evenly
 5 distributed injection rates. (a) permeability 50 mD; (b) permeability 100 mD; (c)
 6 permeability 400 mD.



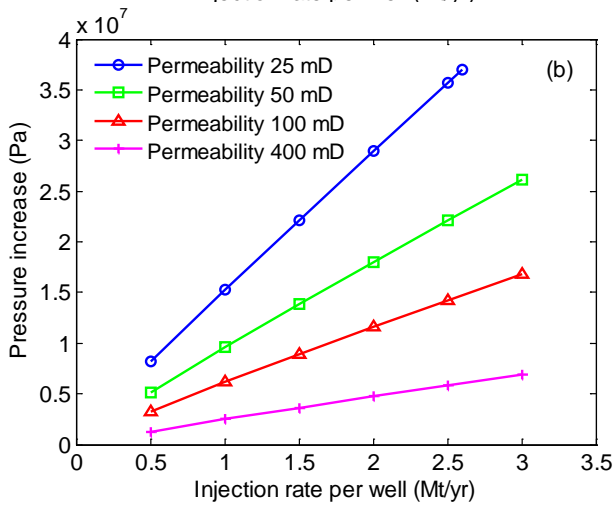
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2 **Fig. 6.** Effect of boundary conditions on the injection pressure.

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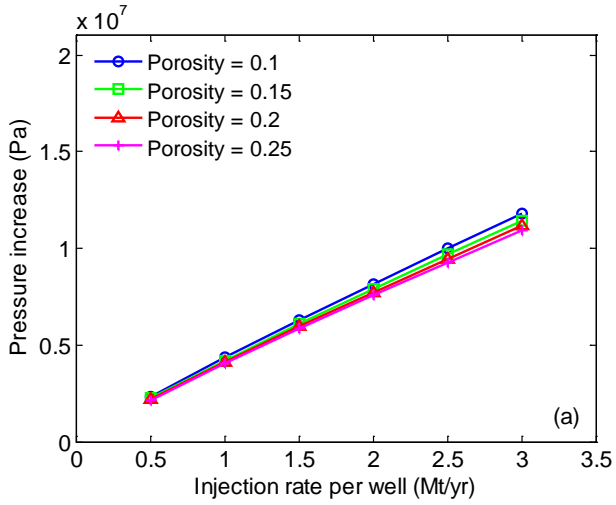
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Fig. 7. Sensitivity of pressure buildup on permeability variation. (a) Romeleåsen Fault

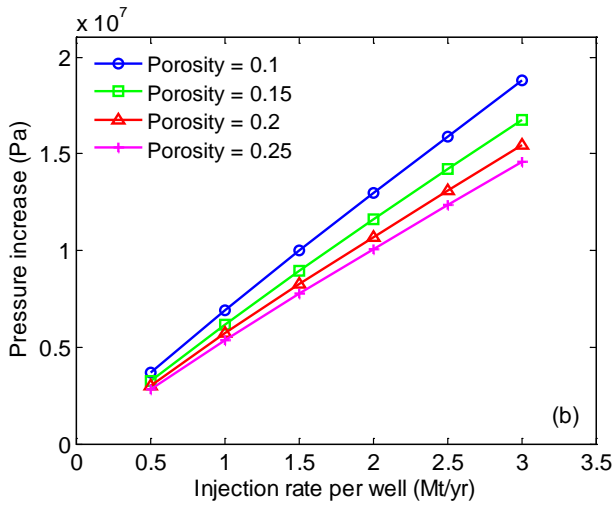
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impermeable; (b) all faults impermeable.

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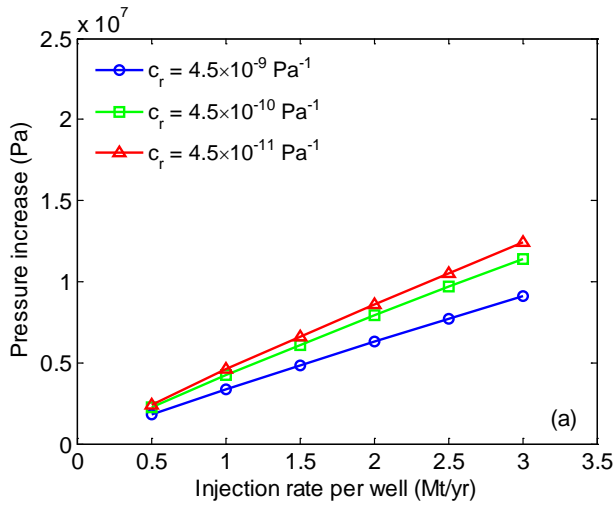
Fig. 8. Sensitivity of pressure buildup on porosity variation. (a) Romeleåsen Fault

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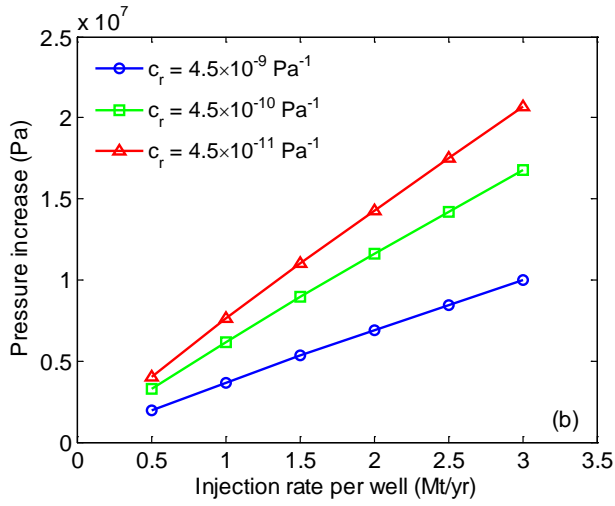
impermeable; (b) all faults impermeable.

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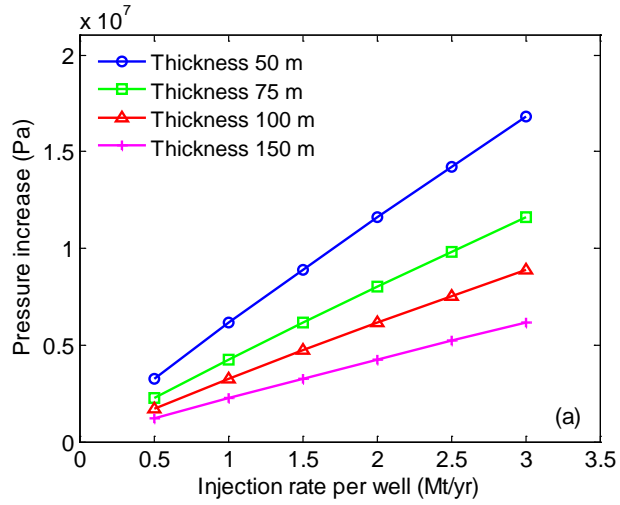
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5 **Fig. 9.** Sensitivity of pressure buildup on rock compressibility variation. (a) Romeleåsen

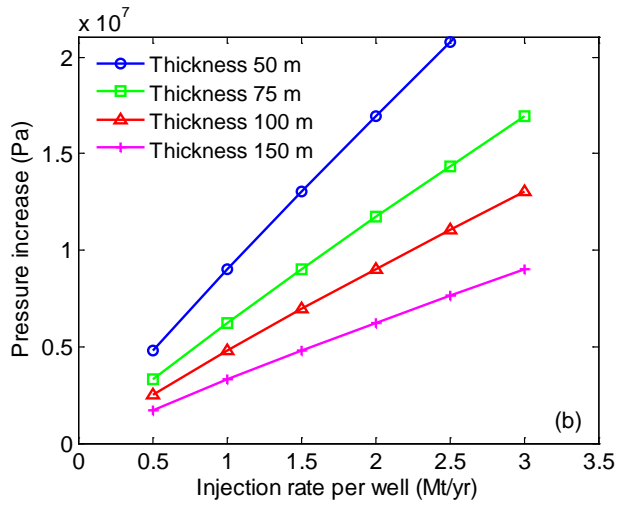
6 Fault impermeable; (b) all faults impermeable.

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4 **Fig. 10.** Sensitivity of pressure buildup on formation thickness variation. (a) Romeleåsen

5 Fault impermeable; (b) all faults impermeable.

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